

اطلاعات آموزشی اطلاعات فنی و مهندسی اخبار روز آب و فاضلاب اخبار استخدامی کارفرمایان



T.me/mohandesifazelab



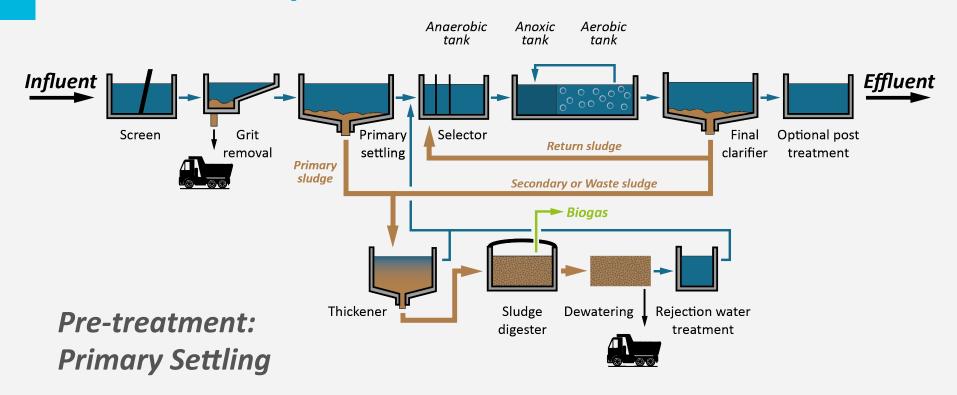
Instagram.com/abfaeng

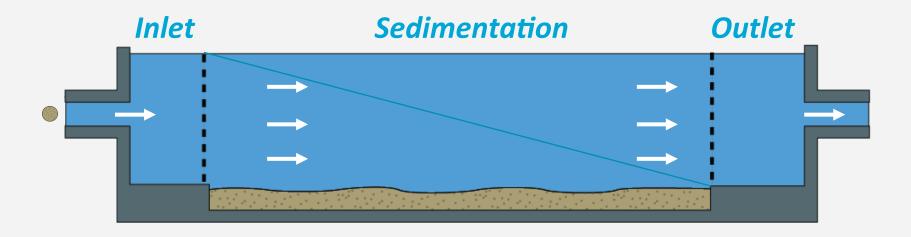
CTB3365x Introduction to water treatment

Prof.dr.ir. Jules B. van Lier

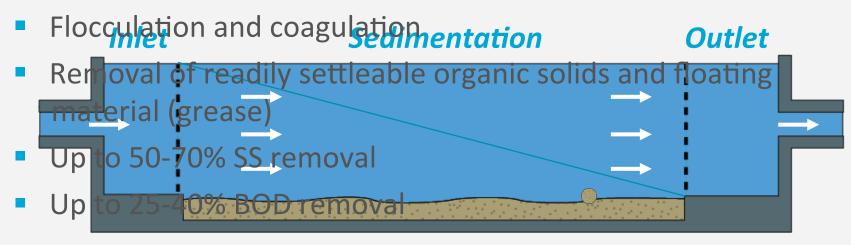


Basic WWTP process units

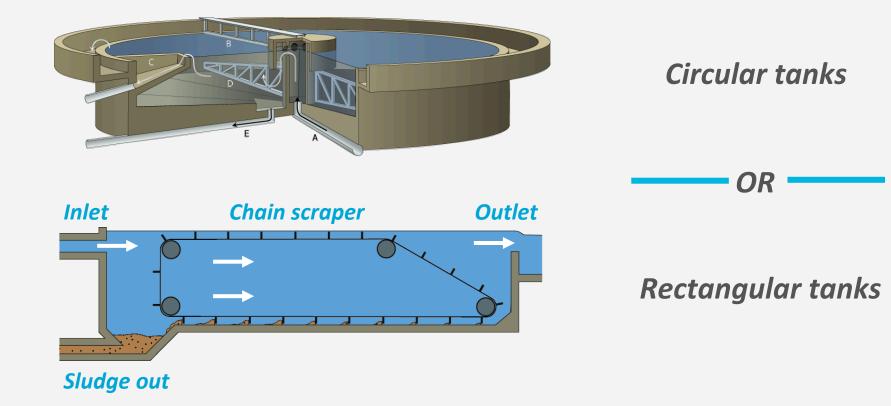




Flocculent and hindered settling



Primary clarifiers



Energy dissipation

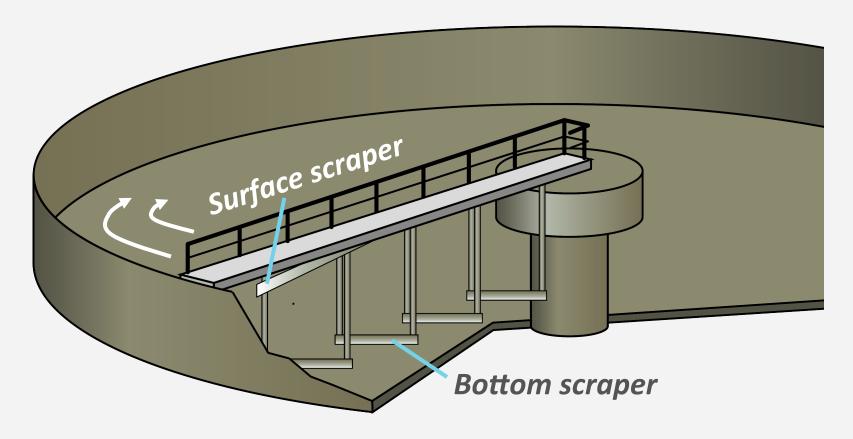




Energy dissipation of incoming flow

• From 0,3..1 *m/s* to 0,03 *m/s*

Circular clarifier





Rectangular tanks







Rectangular tanks







Not allways primary sedimentation!

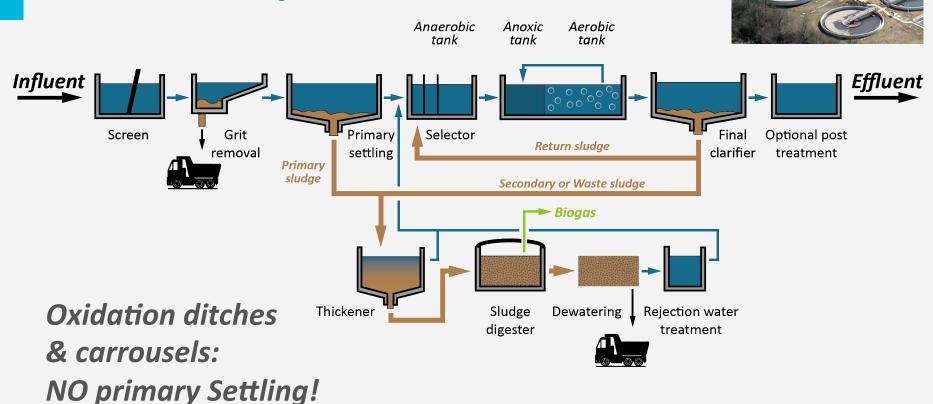
- Oxidation ditches and carrousels are fed with non-clarified raw sewage!
- Primary sludge is stabilised inside the bio-reactor.





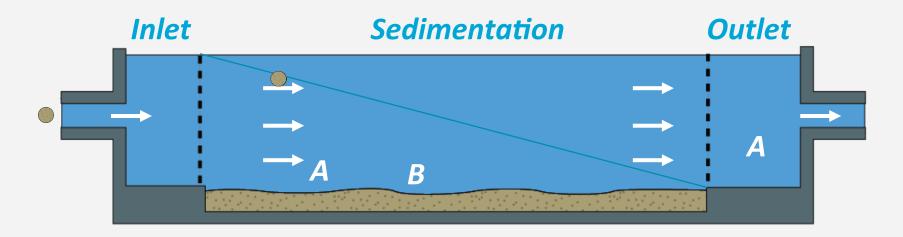


Basic WWTP process units



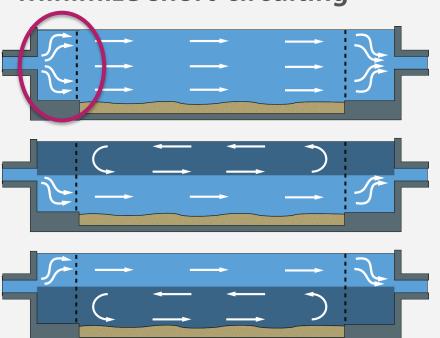
Avoid turbulence:

 $N_R < 1000 - 2000$

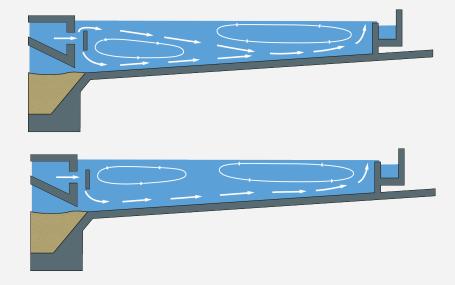


Primary sedimentation, performance

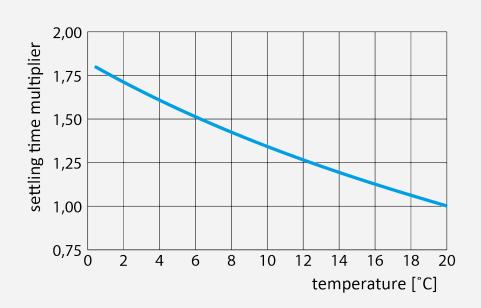
Minimize short-circuiting



Maximize hydraulic stability



Primary sedimentation, temperature



Multiplier: 1.82 ⋅ *e*^{-0.03t}

Viscosity:

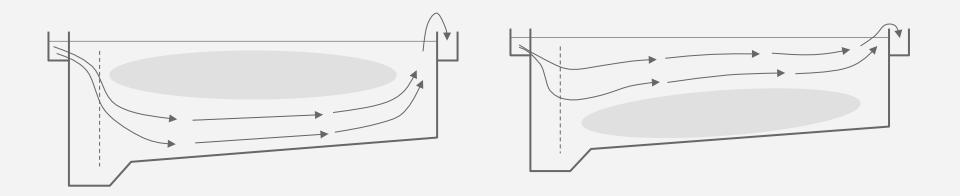
Temp û, μ ↓

$$N_{R} = \frac{v_{O}d_{p}\rho_{w}}{\mu} = \frac{v_{O}d_{p}}{\nu}$$

$$C_{d} = \frac{24}{N_{R}} + \frac{3}{\sqrt{N_{R}}} + 0.34$$

$$v_p = v_o = \sqrt{\frac{4g}{3C_d \varphi} \left(\frac{\rho_p - \rho_w}{\rho_w}\right)} d_p \hat{\mathbf{u}}$$

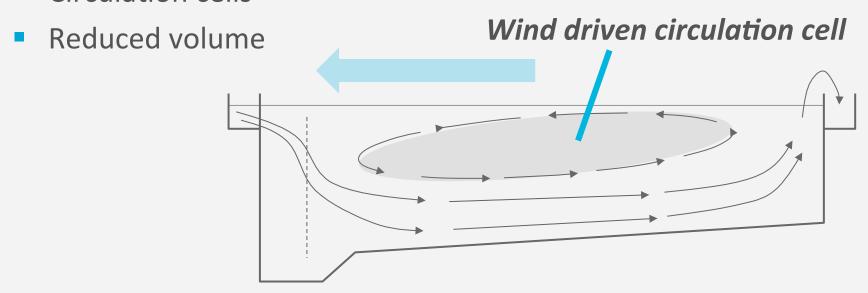
Primary sedimentation, temperature



Primary sedimentation, wind energy

Wind effects:

Circulation cells



Short circuiting & hydraulic stability

Froude number:

• $N_{Fr} > 10^{-5}$; defines subcritical / critical flows, resistance to flow disturbances

$$N_{Fr} = \frac{v_O^2}{g} \frac{L^2(W + 2H)}{WH^3}$$

narrow and long tanks

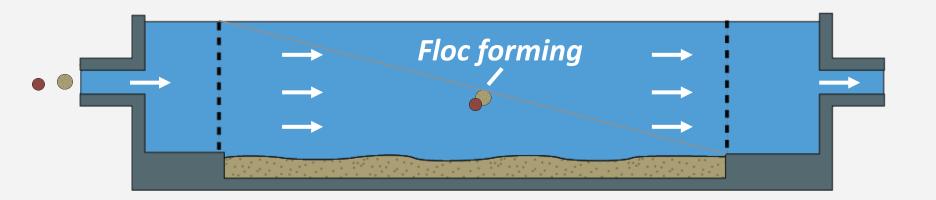
$$N_{Fr} = \frac{v_O^2}{g} \frac{D^4}{64x^2 H}$$

large diameters

Primary sedimentation performance

Detention time and depth:

- Depth: flocculation $(V_p \hat{T})$
 - Depth is important! Not only the hydraulic surface load



Scouring velocity

Depth (H)
$$\downarrow$$
 ------ v_h \uparrow ------ scouring!

$$v_s = v_h = \frac{Q}{W \cdot H}$$

Scouring velocity:
$$v_s = \left(\frac{8k(s-1)gd}{f}\right)^{\frac{1}{2}}$$

v_s = v_h = critical horizontal velocity (m/s) = scouring velocity

d = diameter of particles (m)

s = specific gravity of particles (-)

k = material constant (-)

f = Darcy-Weisbach friction factor (-)

 $g = 9.81 \text{ m/s}^2$

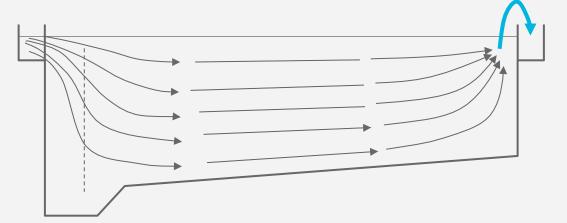
Critical $v_h = v_s$:

- sand: 0.30 m/s
- primary sludge: 0.03 m/s
- activated sludge: 0.02 m/s



Outlet zone:

- Acceleration towards discharge
- Primary sedimentation weir loading: $10-15\frac{m^3}{m \cdot h}$



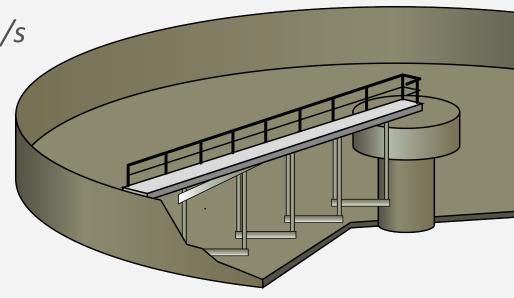
Sludge collection & removal

Sludge collection:

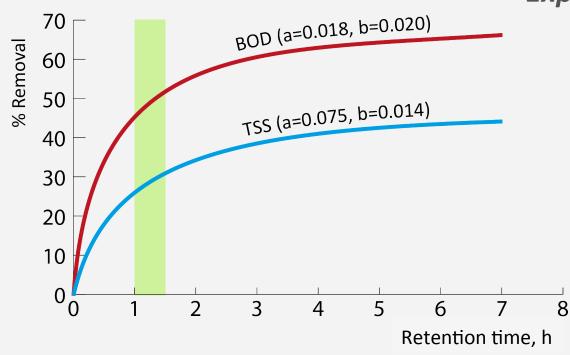
- Bridge speed:
 - Circular: < 0.06 0.07 m/s</p>
 - Rectangular: < 0.03 m/s</p>

Sludge removal:

- (Semi-) Continuous
- Digestion
- Bad odours



BOD and TSS removal efficiency



Expected removal efficiency:

$$R = \frac{t}{a + bt}$$

t = nominal detention time
a,b = empirical constants

Primary sedimentation: Design

General:

- Surface loading rate: $V_0 = \frac{Q}{A} = 1.5 2.5 \frac{m^3}{m^2 \cdot h}$ (max. flow)
 - $\frac{Q}{A} = up \text{ to } 4 \frac{m^3}{m^2 \cdot h} \text{ (max. flow = avg flow (constant))}$
- Hydraulic Residence Time (HRT):
 - Average: 5 h
 - Minimum: approx. 1 1.5 h (during peak flow)
- Water depth: 1.5 2.5 m
- Bottom slope: 1:10 1:12

Primary sedimentation: Design

Circular tanks:

- Diameter:
 - Minimum: 20 m
 - Maximum: 60 m
 - *Optimum:* 30 40 m

Rectangular tanks:

- Maximum length: 90m
 - *Optimum:* 30 50 m
- Width: 5 12 m
 - *Generally:* 5 6 m
- Width:Length: 1:5 1:6
- Depth:Length: 1:20

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